

العنوان:	Heavy Oils Flow in Pipes
المؤلف الرئيسي:	Sakr, Ahmed Lotfy Hassan Rabie
مؤلفين آخرين:	Mousa, Mohamed Ghassoub Saafan, Sultan, Gamal Ibrahim, Talba, Mohamed Abd Almotelb(Super.)
التاريخ الميلادي:	2013
موقع:	المنصورة
الصفحات:	1 - 160
رقم MD:	537574
نوع المحتوى:	رسائل جامعية
اللغة:	Arabic
الدرجة العلمية:	رسالة ماجستير
الجامعة:	جامعة المنصورة
الكلية:	كلية الهندسة
الدولة:	مصر
قواعد المعلومات:	Dissertations
مواضيع:	هندسة القوى الميكانيكية، الزيوت الثقيلة، الأنابيب الموصلة، القوى الميكانيكية
رابط:	https://search.mandumah.com/Record/537574

ملخص الرسالة

إلى عهد قريب قامت الزيوت الخفيفة، كمصدر تقليدي للبتروال الخام، بتوفير احتياجات العالم من مصادر اقتصادية الطاقة، ولكن في السنوات الأخيرة أدت الزيادة الكبيرة في الاستهلاك من المصادر التقليدية للزيت الخام نتيجة لتزايد الطلب على الطاقة، بالإضافة إلى انخفاض الاكتشافات الجديدة مما أدى إلى النقص الشديد في الاحتياطيات المؤكدة من البتروال الخفيف، وضرورة البحث عن مصادر بديلة للطاقة. وتقدم مصادر الزيوت الخام الثقيلة والبيتومين البديل المناسب للطاقة على المدى القصير والبعيد. وتعتبر الزيوت الثقيلة والبيتومين من المصادر الغير تقليدية للطاقة وهي متوفرة على أعماق قريبة من السطح، وتؤكد التقديرات المتحفظة أن المخزون العالمي المؤكد للزيوت الثقيلة يقدر بما يزيد عن ستة تريليون برميل، وتمثل ما يقرب من ٧٠% من الاحتياطيات المؤكدة من مصادر الطاقة في العالم.

وقد أدي النقص الشديد في الاحتياطيات المؤكدة من المصادر التقليدية للبتروال الخام إلى تنامي إنتاج واستخدام الزيوت الثقيلة والعمل على تطوير مصادرها، وتعتبر العقبة الرئيسية في استغلال مصادر الزيوت الثقيلة هي مقاومتها العالية للسريان بسبب اللزوجة الكبيرة لهذه الزيوت والتي قد تصل لآلاف المرات ضعف لزوجة الزيوت الخفيفة، والذي يؤدي بدوره إلى صعوبة أو استحالة نقلها خلال الأنابيب حيث تحتاج إلى طاقة ضخ كبيرة.

وقد استخدمت طرق تكنولوجية مختلفة لنقل الزيوت الثقيلة منها طرق لتخفيض لزوجة الزيت من خلال تسخين خطوط الأنابيب وهي طريقة مكلفة، وخلط الزيوت الثقيلة مع الزيوت الخفيفة أو المنتجات الهيدروكربونية، وفصلها بعد النقل. ويعتبر السريان الحلقي للماء حول الزيوت الثقيلة في أنابيب النقل من أرخص الطرق وأسهل الطرق تكنولوجياً وأكثرها كفاءة، حيث يتم حقن الماء حول الزيت الثقيل مكوناً مجرى حلقي يفصل بين السطح الداخلي لأنبوب النقل والزيت الخام المنقول، ويتميز هذا النوع من السريان بانخفاض المفايد الاحتكاكية والطاقة المطلوبة لضخ الزيت الثقيل، وبالتالي خفض تكلفة نقل الزيوت الثقيلة. ومراجعة الدراسات السابقة تبين الحاجة إلى تقديم دراسات مستفيضة للسريان الحلقي للماء حول الزيوت الثقيلة خلال الأنابيب بغرض توضيح الكثير من الحقائق والمفاهيم المتعلقة بهذا النوع من السريان والحصول على المعلومات التي تساهم في الوصول إلى التصميم الأمثل لخطوط أنابيب النقل للزيوت الثقيلة.

وتقدم هذه الرسالة دراسة عددية للسريان الحلقي للماء حول الزيوت الثقيلة في خطوط الأنابيب الناقلة نتيجة لحقن الماء حلقياً حول الزيت الساري في قلب الأنبوب، بحيث يسري الماء حلقياً فاصلاً الزيت الثقيل عن السطح الداخلي للأنبوب، وذلك بغرض تخفيض المفايد الاحتكاكية، ودراسة تأثير العوامل المختلفة على تطور هيكل السريان، وعلى الفقد في الضغط والنقص في المفايد الاحتكاكية.

وقد استخدم برنامج ديناميكا الموائع الحاسوبية المعروف Fluent 6.3.16 لحل معادلات الحركة للسريان المضطرب للزيوت الثقيلة والماء في أنبوب بقطر ٦ بوصة. وقد تم استخدام عدد كبير من الزيوت الثقيلة تراوحت لزوجتها من ٣٠ إلى ١٨٠٠٠ سنتي بويز. كما تم تغيير نسبة قطر الزيت في قلب الأنبوب إلى القطر الداخلي للأنبوب ٠.٨٣، ٠.٩٢، ٠.٩٦. على الترتيب. كما تم دراسة العوامل المختلفة المؤثرة على تطور التوزيع المقطعي للسرعة، كثافة وطاقة الاضطراب.

وتوضح النتائج أن لزوجة الزيت الثقيل، معدل السريان، نسبة قطر الزيت في القلب إلى قطر الأنبوب، ونسبة كمية الماء إلى كمية الماء والزيت، وسرعة الماء إلى سرعة الزيت عند الدخول لها تأثير كبير على تطور هيكل السريان من لحظة حقن الماء حتى الوصول إلى التطور الكامل، وأنه كلما ارتفعت لزوجة الزيت الثقيل كلما أصبح التطور أسرع. كما توضح النتائج أن توزيع السرعة على أي مقطع كامل التطور أظهر سرعة ثابتة للزيت الثقيل في قلب الأنبوب بينما سرعة الماء في المقطع الحلقي تتغير من صفر على السطح إلى قيمة عظمى عند السطح الفاصل بين الماء والزيت، وأصبح الشكل العام للسريان كما لو كان الزيت الثقيل جسم صلب في قلب الأنبوب يحمله سريان الماء الحلقي المحيط به.

وتؤكد النتائج أن الفقد في الضغط والاحتكاك للسريان الحلقي للماء والزيت الثقيل أقل بكثير من تلك التي تم الحصول عليها في حالة سريان الزيت الثقيل وحده، وأنه تم توفير جزء كبير جداً من الطاقة المستخدمة في ضخ الزيت الثقيل بحقن كمية صغيرة من الماء حول الزيت الثقيل في أنبوب الحقن. كما توضح النتائج أن لزوجة الزيت الثقيل، معدل السريان، نسبة قطر الزيت في القلب إلى قطر الأنبوب، ونسبة كمية الماء إلى كمية الماء والزيت، وسرعة الماء إلى سرعة الزيت عند الدخول تؤثر تأثيراً كبيراً على قيمة الفقد في الضغط ومعامل الاحتكاك مقارنة بتلك المسجلة لسريان الزيوت الثقيلة وحدها في أنبوب النقل، وأنه كلما ارتفعت لزوجة الزيت الثقيل كلما أصبح الفارق بينهما كبيراً.

الرسالة مقدمة في سبعة فصول، إضافة إلى الملخص وقائمة المراجع وملحقين. وقد تم تخصيص الفصل الأول ليعطي مقدمة سريعة للزيت الخام الثقيل موضوع البحث وخصائصه والطرق التكنولوجية المستخدمة لنقله، كما يقدم للسريان الحلقي للماء والزيوت الثقيلة في أنابيب النقل ومدى الحاجة إلى دراسته، وفي الفصل الثاني تم عمل مراجعة للأبحاث السابقة في المجال لتغطي الكثير من الحالات التي تخص ذلك النوع من السريان.

ويغطي الفصل الثالث صياغة النموذج الرياضي المستخلص لتوصيف السريان الحلقي للماء حول الزيت الثقيل في أنبوب النقل، حيث تم توصيف معادلات السريان وكمية الحركة ونموذج الاضطراب المستخدم $k - \omega$ لحل معادلات نافير-ستوكس للسريان الحلقي المضطرب لمائعين مختلفي اللزوجة، كما ناقش الفصل معالجة منطقة السطح والشروط الحدودية. وناقش الفصل الرابع طريقة الحجم المحدودة Finite-volume المستخدمة للحصول على الحل العددي لمعادلات نافير-ستوكس ومعادلات نموذج الاضطراب $k - \omega$ ، كما

يناقش مجموعة برامج ديناميكا الموائع الحاسوبية Fluent CFD Package واستخدامها لتمثيل السريان الحلقي المضطرب للماء حول الزيت الثقيل في أنبوب النقل. ويقدم الفصل الخامس مناقشة لتقييم نتائج النموذج الرياضي مع النتائج العملية المتاحة لبيان صلاحيته وقدرته على معالجة السريان الحلقي للماء حول الزيت الثقيل في أنبوب النقل.

ويقدم الفصل السادس عرض ومناقشة لنتائج دراسة السريان الحلقي للماء والزيت الثقيل في أنبوب النقل، ويناقش هذا الفصل تأثير العوامل المختلفة على تطور هيكل السريان للزيوت الثقيلة في خطوط الأنابيب الناقلة نتيجة لحقن الماء حلقياً حول الزيت الساري في قلب الأنبوب، بحيث يسري الماء حلقياً فاصلاً الزيت الثقيل عن السطح الداخلي للأنبوب، وذلك بغرض تخفيض المفايد الاحتكاكية، كما يناقش تأثير العوامل المختلفة على الفقد في الضغط والنقص في المفايد الاحتكاكية، ويناقش هذا الباب أيضاً التوفير المحقق في الطاقة المستخدمة لضخ الزيوت الثقيلة في خطوط الأنابيب باستخدام طريقة حقن الماء حلقياً حول الزيت الساري في قلب الأنبوب.

وفي النهاية يقدم الفصل السابع من هذه الرسالة ملخصاً سريعاً لموضوع البحث، كما يقدم أهم الاستنتاجات العلمية التي تم استخلاصها من هذه الدراسة، وتختتم الرسالة بأهم المقترحات لاستكمال البحث والدراسات المستقبلية في هذا المجال.

Abstract

Conserved estimates show that heavy oil reserves are estimated to be more than six trillion barrels throughout the world. Their importance tends to increase progressively, as light oil fields are exhausting. The progressive increase of oil demand coupled with the depletion of light crude oils has led to the rapid development of the large world resources of heavy oils. Production of heavy crudes is increasing significantly as low viscosity crudes are depleted. The production of hydrocarbons from heavy oil and bitumen (oil sands) reserves increases annually. The main problem is their high flow resistance caused by the high viscosity. This makes its transportation almost impossible, due to the immense power requirement.

Water lubricated transport of heavy oil is an effective technique for the pipeline transportation of such high viscosity oils. Water is injected into the oil pipelines such that it flows as annular film encapsulating the oil in the core region. Such flow is well known as oil-water core annular pipe flow. Water is acting as lubricant for heavy oils transport in pipeline. Since oil does not come in contact with the wall, the wall shear is comparable to the shear encountered during the flow of water in the pipe. This reduces drastically the pumping power and the cost of transportation of heavy oil and bitumen.

Literature review reveals that there is limited number of numerical studies concerning the core annular flows of heavy oils and water. Many aspects need to be clarified such as flow structure and the influence of different parameters on pressure reduction. In this work, study of the core annular flow of heavy oils and water in a pipe is presented. Numerical simulation of the axisymmetric laminar core, turbulent annular flow is carried out using the standard $k-\omega$ model. The flow field and flow characteristics are investigated using Fluent 6.32 CFD package. The core annular flow of heavy oils water in 15.24 cm diameter pipe is considered. The influence of different core annular flow parameters upon pressure gradient and friction coefficient is investigated. Flow parameters considered are flow Reynolds number, oil to water

viscosity ratio, water to oil volume ratio, core to pipe diameters ratio, and oil and water superficial velocity. Oil and water flow development is also investigated.

Flow structure investigation demonstrated that major changes in flow structure occur at the oil-water interface. The fully-developed velocity profile of oil-water core annular flow exhibits distinguishable core and annular regions, and the oil velocity profile in the core region is almost constant with little variations, while in the annulus it looks like a turbulent one with sharp increase near the wall to maximum at oil-water interface. For heavy oils with viscosity $\mu > 3000$ cP, velocity profile exhibits constant distribution in the oil core and the core looks like a rigid body carried by the annular water flow.

Results show that the pressure drop and friction losses of the oil-water core annular flow is much smaller compared to those of oils flowing alone in the pipeline. That means saving a lot of pumping power is achieved when injecting small amount of water to encapsulate heavy oil in the pipe core. Results of oil-water core annular flow exhibit better reduction in friction loss in pipes with thicker water annulus.

It has been demonstrated that friction coefficient C_f of heavy oil pipe flow, as single phase, is in full agreement with the well-known Blasius relation $C_f = 16/Re$. For the results presented in this work, the friction coefficient C_f of the heavy oil-water core annular flow is best fitted by the relation $C_f = 0.003 \cdot Re_o^{0.012}$.

Results show that the reduction in pressure gradient ratio Φ and friction coefficient ratio β of oil-water flow increases with the viscosity of the heavy oil μ_r . The pressure gradient ratio Φ is best fitted to oil's viscosity (μ_r) by the relation $\Phi = 0.126 \cdot [\mu_r]^{0.7}$, whereas the friction coefficient ratio β is best fitted by $\beta = 0.083 \cdot [\mu_r]^{0.77}$. The results of Φ , and β are best fitted to oil based Reynolds number as, $\Phi = 1016/Re_o^{0.71}$ and $\beta = 1515/Re_o^{0.77}$ showing that they are inversely proportional to the relative viscosity μ_r

العنوان:	Heavy Oils Flow in Pipes
المؤلف الرئيسي:	Sakr, Ahmed Lotfy Hassan Rabie
مؤلفين آخرين:	Mousa, Mohamed Ghassoub Saafan, Sultan, Gamal Ibrahim, Talba, Mohamed Abd Almotelb(Super.)
التاريخ الميلادي:	2013
موقع:	المنصورة
الصفحات:	1 - 160
رقم MD:	537574
نوع المحتوى:	رسائل جامعية
اللغة:	Arabic
الدرجة العلمية:	رسالة ماجستير
الجامعة:	جامعة المنصورة
الكلية:	كلية الهندسة
الدولة:	مصر
قواعد المعلومات:	Dissertations
مواضيع:	هندسة القوى الميكانيكية، الزيوت الثقيلة، الأنابيب الموصلة، القوى الميكانيكية
رابط:	https://search.mandumah.com/Record/537574

Table of Contents

Acknowledgments	i
Abstract	ii
Table of Contents	iv
List of Figures	vii
List of Tables	xiv
Nomenclature	xv
Chapter 1: Introduction	1
1.1 Introduction	1
1.2 Crude Oils Classification	2
1.3 Heavy Oils and Bitumen World’s Reserve Estimates	4
1.4 Heavy Oils Transportation	6
1.5 Thesis Outlines	8
Chapter 2: Literature Review	10
2.1 Introduction	10
2.2 Water Lubricated Transport of Heavy Oils	10
2.3 Core Annular Pipe Flow of Heavy Oils	13
2.3.1 Core Annular Flow in Horizontal Pipes.....	14
2.3.2 Core Annular Flow in Vertical Pipes.....	18
2.3.3 Core Annular Flow Numerical Modeling.....	19
2.3.4 Stability of Core Annular Flow	21
2.4 Fouling in Water Lubricated Heavy Oils Flow.....	23
2.5 Self-Lubricated Heavy Oils Flow	24
2.6 Heavy Oils Transport Using Drag Reducing Additives	25
2.7 Work Objectives.....	26
Chapter 3: Mathematical Formulation	28
3.1 Introduction	28
3.2 Physical Description of the Problem	29
3.3 The Governing Equations.....	31
3.3.1 Continuity Equation.....	31
3.3.2 Momentum Equation.....	31
3.3.3 Fluid Constitutive Equations	32

Table of Contents

3.4 Navier-Stokes Equations.....	32
3.5 Turbulent Flow Modeling	33
3.5.1 Reynolds-Averaging of Navier-Stokes Equations.....	33
3.5.2 Boussinesq Approach	34
3.5.3 The Two-Equation Models of Turbulence	35
3.6 The Standard k- ω Model	36
3.6.1 Transport Equations for the Standard k- ω Model	37
3.6.2 Modeling the Turbulence Production	38
3.6.3 Modeling the Turbulence Dissipation	39
3.6.4 Model Constants	40
3.7 Wall Treatment in k- ω Turbulence Model	40
3.8 Problem Boundary Conditions	42
Chapter 4: Numerical Technique and Procedure	45
4.1 Introduction	45
4.2 Overview of the Numerical Procedure.....	45
4.3 The Finite-Volume Method.....	47
4.4 Discretization of PDE.....	48
4.5 Pressure-Velocity Coupling.....	48
4.6 Procedures for the Flow Field Predictions.....	49
4.7 Fluent CFD Package.....	49
4.8 Simulation Setup and Meshing Techniques.....	50
4.9 Simulation Procedure.....	54
Chapter 5: Numerical Model Verification	57
5.1 Introduction.....	57
5.2 Laminar Velocity Distribution Predictions.....	57
5.3 Turbulent Velocity Distribution Predictions.....	59
5.4 Friction Coefficient Predictions of Fully-Developed Pipe Flow.....	63
Chapter 6: Results and Discussions	65
6.1 Introduction.....	65
6.2 Oil-Water Core Annular Flow Structure Development	67
6.2.1 Flow Velocity Profiles Development	67
6.2.1.1 Axial Velocity Profiles.....	67
6.2.1.2 Radial Velocity Profiles.....	80

Table of Contents

6.2.2 Effect of Water Loading on Oil-Water Velocity Profiles.....	84
6.2.3 Oil-Water Turbulence Kinetic Energy “ k ” Profiles.....	91
6.2.4 Strain Rate γ Profiles of Oil-Water Core Annular Flow.....	99
6.3 Flow Structure at Oil-Water Interface.....	102
6.3.1 Axial Velocity at Oil-Water Interface.....	102
6.3.2 Strain Rate γ at Oil-Water interface.....	103
6.3.3 Turbulence Kinetic Energy k and Turbulence Intensity I	104
6.4 Axial Development of Flow Parameters.....	109
6.4.1 Development of Axial Velocity at Pipe Centerline.....	109
6.4.2 Development of Wall Shear Stress τ_w	110
6.4.3 Development of Friction Coefficient C_f	112
6.4.4 Development of Static Pressure.....	113
6.5 Flow Characteristics of Oil-Water Core Annular Flow	115
6.5.1 Effect of Water Loading ψ on Pressure Drop and Friction Loss.....	116
6.5.1.1 Effect of Water Loading Ratio ψ on Pressure Gradient dp/dx	116
6.5.1.2 Effect of Water Loading Ratio ψ on Friction Coefficient C_f	120
6.5.2 Effect of Mass Flow Rate on Pressure Drop and Friction Loss.....	124
6.5.2.1 Effect of Mass Flow Rate on Pressure Gradient	124
6.5.2.2 Effect of Mass Flow Rate on Friction Coefficient C_f	126
6.5.3 Effect of Heavy Oil’s Viscosity on Pressure Drop and Friction Loss.....	129
6.6 Pumping Power of Oil-Water Core Annular Flow	140
6.5.1 Effect of Water Loading ψ on Pumping Power.....	140
6.5.2 Effect of Mass Flow Rate on Pumping Power.....	143
6.5.3 Effect of Heavy Oil’s Viscosity on Pumping Power.....	145
Chapter 7: Conclusions and Recommendations.....	150
7.1 Conclusions.....	150
7.2 Recommendations for Future Studies	152
References.....	153
Appendix A: Discretization of Governing Equations	A-1
Appendix B: Pressure-Velocity Coupling and SIMPLE Algorithm	B-1

العنوان:	Heavy Oils Flow in Pipes
المؤلف الرئيسي:	Sakr, Ahmed Lotfy Hassan Rabie
مؤلفين آخرين:	Mousa, Mohamed Ghassoub Saafan, Sultan, Gamal Ibrahim, Talba, Mohamed Abd Almotelb(Super.)
التاريخ الميلادي:	2013
موقع:	المنصورة
الصفحات:	1 - 160
رقم MD:	537574
نوع المحتوى:	رسائل جامعية
اللغة:	Arabic
الدرجة العلمية:	رسالة ماجستير
الجامعة:	جامعة المنصورة
الكلية:	كلية الهندسة
الدولة:	مصر
قواعد المعلومات:	Dissertations
مواضيع:	هندسة القوى الميكانيكية، الزيوت الثقيلة، الأنابيب الموصلة، القوى الميكانيكية
رابط:	https://search.mandumah.com/Record/537574

*Mansoura University
Faculty of Engineering
Mechanical Power Engineering Dept.*



Heavy Oils Flow in Pipes

by

Eng. Ahmed Lotfy Hassan Rabie Sakr

B.Sc. Mechanical Power Engineering 2005

A Thesis

Submitted to the Faculty of Engineering, Mansoura University
in Partial Fulfillment of the Requirements for the
Degree of Master of Science (M.Sc.)

in

Mechanical Power Engineering

Supervised by

Prof. Dr. Gamal Ibrahim Sultan
Professor
Mechanical Engineering Dept.
Mansoura University

Prof. Dr. Mohamed Ghassob Mousa
Professor
Mechanical Engineering Dept.
Mansoura University

Dr. Mohamed Abdel Motelb Tolba
Assistant Professor, Mechanical Engineering Dept.
Mansoura University

2013

Mansoura University
Faculty of Engineering
Mechanical Engineering Department



Supervision Committee

Degree: M.Sc. Degree

Thesis Title: Heavy Oils Flow in Pipes

Researcher Name: Ahmed Lotfy Hassan Rabie Sakr

Supervisors:

Name	Position	Signature
Prof. Dr. Gamal I. Sultan	<i>Professor of Mechanical Engineering Mechanical Power Engineering Dept. Faculty of Engineering – Mansoura University</i>	
Prof. Dr. Mohamed Ghassob S. Mousa	<i>Professor of Mechanical Engineering Mechanical Power Engineering Dept. Faculty of Engineering – Mansoura University</i>	
Dr. Mohamed A. Tolba	<i>Assistant Professor of Mechanical Engineering Mechanical Power Engineering Dept. Faculty of Engineering – Mansoura University</i>	

**Head, Mechanical Power
Engineering Dept.**

**Prof. Dr
Mohamed Nabil Sabry**

**Vice Dean for
Post Graduate Studies**

**Prof. Dr
Kasem Salah El Alfy**

**Dean,
Faculty of Engineering**

**Prof. Dr.
Zaki M. Zedan**



Examination Committee

Degree: M.Sc. Degree

Thesis Title: Heavy Oils Flow in Pipes

Researcher Name: Ahmed Lotfy Hassan Rabie Sakr

Supervision Committee:

Name	Position	Signature
Prof. Dr. Gamal I. Sultan	Professor, Mechanical Power Engineering Dept. Faculty of Engineering – Mansoura University	
Prof. Dr. Mohamed Ghassob S. Mousa	Professor, Mechanical Power Engineering Dept. Faculty of Engineering – Mansoura University	
Dr. Mohamed A. Tolba	Assistant Professor, Mechanical Power Engineering Dept. Faculty of Engineering – Mansoura University	

Examination Committee:

Name	Position	Signature
Prof. Dr. Kamal Abdul Aziz Ibrahim	Professor, Mechanical Engineering Dept. Faculty of Engineering, Menofia University	
Prof. Dr. Berge O. Djebedjian	Professor, Mechanical Power Engineering Dept. Faculty of Engineering, Mansoura University	
Prof. Dr. Gamal I. Sultan	Professor, Mechanical Power Engineering Dept. Faculty of Engineering, Mansoura University	
Prof. Dr. Mohamed Ghassob S. Mousa	Professor, Mechanical Power Engineering Dept. Faculty of Engineering – Mansoura University	

Head, Mechanical Power Engineering Dept.

Prof. Dr. Mohamed Nabil Sabry

Vice Dean for Post Graduate Studies

Prof. Dr. Kasem Salah El Alfy

Dean, Faculty of Engineering

Prof. Dr. Zaki M. Zedan

Dedication

To my father *Prof. Dr. Lotfy Sakr* for being a wonderful dad

Specially dedicated to my wife, *Amany El-Shal*, for her support and encouragement during the time when I was busy with my studies, and to my little angles *Hala* and *Marawan*.

ACKNOWLEDGEMENTS

First of all, I thank Allah Almighty for his grace, favour and most of all his peace throughout the completion of this study. In him and through him, I have accomplished all that I set out to do.

My deepest and sincere thanks go to Prof. Dr. Gamal I. Sultan for his patience, guidance and invaluable advice towards the completion of this work. Special thanks go to Prof. Dr. Mohamed Ghassob Saafan Mousa for his invaluable advice and continuous support all the time. My deepest and sincere thanks go also to Dr. Mohamed A. Tolba for his helpful suggestions and continuous support during the course of this work and my undergraduate studying.

My sincere thanks and appreciation go to my pillar of strength, my father, Prof. Dr. Lotfy H. Rabie for his helpful discussions and continuous support all the time. His encouragements and words of wisdom will continue to motivate me in my career.

My deepest love and gratitude go to my wonderful brother Eng. Mohamed for his helpful discussions, continuous support and encouragement, to my wife Amany for patience, constant support and encouragement in the hard times.

My thanks go to the Faculty and staff of the Mechanical Power Engineering Department, Mansoura University for their moral and technical support during all my studying period.

My deepest and sincere thanks go to my friends and colleagues who offered me their moral support and encouragements. Special thanks and appreciation go to my department manager Eng. Mohamed Mostafa, for his moral and technical support.

Finally, thanks for anybody puts an obstacle in my way to stop me, it was a strong motivation for me to success in my life.

Abstract

Conserved estimates show that heavy oil reserves are estimated to be more than six trillion barrels throughout the world. Their importance tends to increase progressively, as light oil fields are exhausting. The progressive increase of oil demand coupled with the depletion of light crude oils has led to the rapid development of the large world resources of heavy oils. Production of heavy crudes is increasing significantly as low viscosity crudes are depleted. The production of hydrocarbons from heavy oil and bitumen (oil sands) reserves increases annually. The main problem is their high flow resistance caused by the high viscosity. This makes its transportation almost impossible, due to the immense power requirement.

Water lubricated transport of heavy oil is an effective technique for the pipeline transportation of such high viscosity oils. Water is injected into the oil pipelines such that it flows as annular film encapsulating the oil in the core region. Such flow is well known as oil-water core annular pipe flow. Water is acting as lubricant for heavy oils transport in pipeline. Since oil does not come in contact with the wall, the wall shear is comparable to the shear encountered during the flow of water in the pipe. This reduces drastically the pumping power and the cost of transportation of heavy oil and bitumen.

Literature review reveals that there is limited number of numerical studies concerning the core annular flows of heavy oils and water. Many aspects need to be clarified such as flow structure and the influence of different parameters on pressure reduction. In this work, study of the core annular flow of heavy oils and water in a pipe is presented. Numerical simulation of the axisymmetric laminar core, turbulent annular flow is carried out using the standard $k-\omega$ model. The flow field and flow characteristics are investigated using Fluent 6.32 CFD package. The core annular flow of heavy oils water in 15.24 cm diameter pipe is considered. The influence of different core annular flow parameters upon pressure gradient and friction coefficient is investigated. Flow parameters considered are flow Reynolds number, oil to water

viscosity ratio, water to oil volume ratio, core to pipe diameters ratio, and oil and water superficial velocity. Oil and water flow development is also investigated.

Flow structure investigation demonstrated that major changes in flow structure occur at the oil-water interface. The fully-developed velocity profile of oil-water core annular flow exhibits distinguishable core and annular regions, and the oil velocity profile in the core region is almost constant with little variations, while in the annulus it looks like a turbulent one with sharp increase near the wall to maximum at oil-water interface. For heavy oils with viscosity $\mu > 3000$ cP, velocity profile exhibits constant distribution in the oil core and the core looks like a rigid body carried by the annular water flow.

Results show that the pressure drop and friction losses of the oil-water core annular flow is much smaller compared to those of oils flowing alone in the pipeline. That means saving a lot of pumping power is achieved when injecting small amount of water to encapsulate heavy oil in the pipe core. Results of oil-water core annular flow exhibit better reduction in friction loss in pipes with thicker water annulus.

It has been demonstrated that friction coefficient C_f of heavy oil pipe flow, as single phase, is in full agreement with the well-known Blasius relation $C_f = 16/Re$. For the results presented in this work, the friction coefficient C_f of the heavy oil-water core annular flow is best fitted by the relation $C_f = 0.003 \cdot Re_o^{0.012}$.

Results show that the reduction in pressure gradient ratio Φ and friction coefficient ratio β of oil-water flow increases with the viscosity of the heavy oil μ_r . The pressure gradient ratio Φ is best fitted to oil's viscosity (μ_r) by the relation $\Phi = 0.126 \cdot [\mu_r]^{0.7}$, whereas the friction coefficient ratio β is best fitted by $\beta = 0.083 \cdot [\mu_r]^{0.77}$. The results of Φ , and β are best fitted to oil based Reynolds number as, $\Phi = 1016/Re_o^{0.71}$ and $\beta = 1515/Re_o^{0.77}$ showing that they are inversely proportional to the relative viscosity μ_r

Table of Contents

Acknowledgments	i
Abstract	ii
Table of Contents	iv
List of Figures	vii
List of Tables	xiv
Nomenclature	xv
Chapter 1: Introduction	1
1.1 Introduction	1
1.2 Crude Oils Classification	2
1.3 Heavy Oils and Bitumen World’s Reserve Estimates	4
1.4 Heavy Oils Transportation	6
1.5 Thesis Outlines	8
Chapter 2: Literature Review	10
2.1 Introduction	10
2.2 Water Lubricated Transport of Heavy Oils	10
2.3 Core Annular Pipe Flow of Heavy Oils	13
2.3.1 Core Annular Flow in Horizontal Pipes.....	14
2.3.2 Core Annular Flow in Vertical Pipes.....	18
2.3.3 Core Annular Flow Numerical Modeling.....	19
2.3.4 Stability of Core Annular Flow	21
2.4 Fouling in Water Lubricated Heavy Oils Flow.....	23
2.5 Self-Lubricated Heavy Oils Flow	24
2.6 Heavy Oils Transport Using Drag Reducing Additives	25
2.7 Work Objectives.....	26
Chapter 3: Mathematical Formulation	28
3.1 Introduction	28
3.2 Physical Description of the Problem	29
3.3 The Governing Equations.....	31
3.3.1 Continuity Equation.....	31
3.3.2 Momentum Equation.....	31
3.3.3 Fluid Constitutive Equations	32

Table of Contents

3.4 Navier-Stokes Equations.....	32
3.5 Turbulent Flow Modeling	33
3.5.1 Reynolds-Averaging of Navier-Stokes Equations.....	33
3.5.2 Boussinesq Approach	34
3.5.3 The Two-Equation Models of Turbulence	35
3.6 The Standard k - ω Model	36
3.6.1 Transport Equations for the Standard k - ω Model	37
3.6.2 Modeling the Turbulence Production	38
3.6.3 Modeling the Turbulence Dissipation	39
3.6.4 Model Constants	40
3.7 Wall Treatment in k - ω Turbulence Model	40
3.8 Problem Boundary Conditions	42
Chapter 4: Numerical Technique and Procedure	45
4.1 Introduction	45
4.2 Overview of the Numerical Procedure.....	45
4.3 The Finite-Volume Method.....	47
4.4 Discretization of PDE.....	48
4.5 Pressure-Velocity Coupling.....	48
4.6 Procedures for the Flow Field Predictions.....	49
4.7 Fluent CFD Package.....	49
4.8 Simulation Setup and Meshing Techniques.....	50
4.9 Simulation Procedure.....	54
Chapter 5: Numerical Model Verification	57
5.1 Introduction.....	57
5.2 Laminar Velocity Distribution Predictions.....	57
5.3 Turbulent Velocity Distribution Predictions.....	59
5.4 Friction Coefficient Predictions of Fully-Developed Pipe Flow.....	63
Chapter 6: Results and Discussions	65
6.1 Introduction.....	65
6.2 Oil-Water Core Annular Flow Structure Development	67
6.2.1 Flow Velocity Profiles Development	67
6.2.1.1 Axial Velocity Profiles.....	67
6.2.1.2 Radial Velocity Profiles.....	80

Table of Contents

6.2.2 Effect of Water Loading on Oil-Water Velocity Profiles.....	84
6.2.3 Oil-Water Turbulence Kinetic Energy “ k ” Profiles.....	91
6.2.4 Strain Rate γ Profiles of Oil-Water Core Annular Flow.....	99
6.3 Flow Structure at Oil-Water Interface.....	102
6.3.1 Axial Velocity at Oil-Water Interface.....	102
6.3.2 Strain Rate γ at Oil-Water interface.....	103
6.3.3 Turbulence Kinetic Energy k and Turbulence Intensity I	104
6.4 Axial Development of Flow Parameters.....	109
6.4.1 Development of Axial Velocity at Pipe Centerline.....	109
6.4.2 Development of Wall Shear Stress τ_w	110
6.4.3 Development of Friction Coefficient C_f	112
6.4.4 Development of Static Pressure.....	113
6.5 Flow Characteristics of Oil-Water Core Annular Flow	115
6.5.1 Effect of Water Loading ψ on Pressure Drop and Friction Loss.....	116
6.5.1.1 Effect of Water Loading Ratio ψ on Pressure Gradient dp/dx	116
6.5.1.2 Effect of Water Loading Ratio ψ on Friction Coefficient C_f	120
6.5.2 Effect of Mass Flow Rate on Pressure Drop and Friction Loss.....	124
6.5.2.1 Effect of Mass Flow Rate on Pressure Gradient	124
6.5.2.2 Effect of Mass Flow Rate on Friction Coefficient C_f	126
6.5.3 Effect of Heavy Oil’s Viscosity on Pressure Drop and Friction Loss.....	129
6.6 Pumping Power of Oil-Water Core Annular Flow	140
6.5.1 Effect of Water Loading ψ on Pumping Power.....	140
6.5.2 Effect of Mass Flow Rate on Pumping Power.....	143
6.5.3 Effect of Heavy Oil’s Viscosity on Pumping Power.....	145
Chapter 7: Conclusions and Recommendations.....	150
7.1 Conclusions.....	150
7.2 Recommendations for Future Studies	152
References.....	153
Appendix A: Discretization of Governing Equations	A-1
Appendix B: Pressure-Velocity Coupling and SIMPLE Algorithm	B-1

List of Figures

Figure (1.1):	Classification of crude oils according to viscosity and API gravity	3
Figure (1.2a):	World's reserves of conventional crude and resources of heavy oil and bitumen	4
Figure (1.2b):	Total estimated world's oil reserves	5
Figure (3.1):	Schematic description of the core annular pipe flow	30
Figure (3.2):	Flow geometry and coordinate system	30
Figure (3.3):	Computational domain and boundary conditions	43
Figure (4.1):	Overview of the numerical procedure	46
Figure (4.2):	Core annular flow computational domain and the coordinate system ...	51
Figure (4.3):	Grid structure of the 2D axisymmetric core annulus pipe flow	52
Figure (4.4a):	Flow simulation convergence plot using First Order Scaled Residuals...	55
Figure (4.4b):	Flow simulation convergence plot using QUICK Scaled Residuals	56
Figure (5.1):	Development of velocity profiles in the heavy oil ($\mu=3244$ cP) at $Re=75$	58
Figure (5.2):	Velocity profiles of fully development laminar pipe flow of heavy oils..	59
Figure (5.3):	Typical velocity distribution for the near-wall region and outer layer of turbulent boundary layer flow	60
Figure (5.4):	Predicted velocity distribution U^+ as function of wall distance y^+ for turbulent pipe flow, at Reynolds number ($Re=13106$ and 60868)	62
Figure (5.5):	Velocity profile predictions compared with the experimental data of Zagarola and Smits (1997), Escudier and Presti [sited in Gibbings (1996)]	62
Figure (5.6):	Friction coefficient (C_f) vs. Reynolds number (Re) in the fully-developed pipe flow	63
Figure (6.1a):	Axial velocity profiles development of core annular pipe flow of oil-water system $\alpha = 0.83$, $U_o=U_w=2$ m/s, Mineral Oil ($\mu=30$ cP)	69
Figure (6.1b):	Velocity profiles development of core annular pipe flow of oil-water system $\alpha = 0.83$, $U_o = U_w = 2$ m/s, Heavy oil 4 ($\mu=84$ cP)	69
Figure (6.1c):	Axial velocity profiles development of core annular pipe flow of oil-water system $\alpha = 0.83$, $U_o = U_w = 2$ m/s, Crude oil ($\mu=530$ cP)	71
Figure (6.1d):	Axial velocity profiles development of core annular pipe flow of oil-water system $\alpha = 0.83$, $U_o = U_w = 2$ m/s, Engine oil ($\mu=1060$ cP)	71

List of Figures

Figure (6.1e):	Axial velocity profiles development of core annular pipe flow of oil-water system $\alpha = 0.83$, $U_o = U_w = 2$ m/s, Heavy oil ($\mu=3244$ cP)	73
Figure (6.1f):	Axial velocity profiles development of core annular pipe flow of oil-water system $\alpha = 0.83$, $U_o = U_w = 2$ m/s, Fuel oil ($\mu=18000$ cP)	73
Figure (6.2a):	Axial velocity profiles development of core annular pipe flow of oil-water system $\alpha = 0.96$, $U_o = U_w = 3$ m/s, Mineral oil ($\mu=30$ cP)	75
Figure (6.2b):	Axial velocity profiles development of core annular pipe flow of oil-water system $\alpha = 0.96$, $U_o = U_w = 3$ m/s, Heavy oil ($\mu=157$ cP)	75
Figure (6.2c):	Axial velocity profiles development of core annular pipe flow of oil-water system $\alpha = 0.96$, $U_o = U_w = 3$ m/s, Heavy oil ($\mu=621$ cP)	77
Figure (6.2d):	Axial velocity profiles development of core annular pipe flow of oil-water system $\alpha = 0.96$, $U_o = U_w = 3$ m/s, Heavy oil ($\mu=1318$ cP)	77
Figure (6.2e):	Axial velocity profiles development of core annular pipe flow of oil-water system $\alpha = 0.96$, $U_o = U_w = 3$ m/s, Heavy oil ($\mu=10230$ cP).....	79
Figure (6.2f):	Axial velocity profiles development of core annular pipe flow of oil-water system $\alpha = 0.96$, $U_o = U_w = 3$ m/s, Fuel oil ($\mu=18000$ cP)	79
Figure (6.3a):	Radial velocity profiles development of core annular pipe flow of oil-water system $\alpha = 0.92$, $U_o = U_w = 3$ m/s, Mineral oil ($\mu=30$ cP)	81
Figure (6.3b):	Radial velocity profiles development of core annular pipe flow of oil-water system $\alpha = 0.92$, $U_o = U_w = 3$ m/s, Heavy oil 2($\mu=621$ cP)	81
Figure (6.3c):	Radial velocity profiles development of core annular pipe flow of oil-water system $\alpha = 0.92$, $U_o = U_w = 3$ m/s, Crude oil 7 ($\mu=1935$ cP)	83
Figure (6.3d):	Radial velocity profiles development of core annular pipe flow of oil-water system $\alpha = 0.92$, $U_o = U_w = 3$ m/s, Extra Heavy oil HO7 ($\mu=10230$ cP)	83
Figure (6.3e):	Radial velocity profiles development of core annular pipe flow of oil-water system $\alpha = 0.92$, $U_o = U_w = 3$ m/s, Fuel oil ($\mu=18000$ cP)	84
Figure (6.4a):	Axial velocity profiles of heavy oil-water core annular pipe flow, Engine oil ($\mu = 1060$ cP), $\alpha = 0.92$, Water loading $\psi = 0.04$, $U_o = 2$ m/s, $U_w = 0.5$ m/s	86
Figure (6.4b):	Axial velocity profiles of heavy oil-water core annular pipe flow, Engine oil ($\mu = 1060$ cP), $\alpha = 0.92$, Water loading $\psi = 0.08$, $U_o = 2$ m/s, $U_w = 1$ m/s	87
Figure (6.4c):	Axial velocity profiles of heavy oil-water core annular pipe flow, Engine oil ($\mu = 1060$ cP), $\alpha = 0.92$, Water loading $\psi = 0.12$, $U_o = 2$ m/s, $U_w = 1.50$ m/s	88
Figure (6.4d):	Axial velocity profiles of heavy oil-water core annular pipe flow, Engine oil ($\mu = 1060$ cP), $\alpha = 0.92$, Water loading $\psi = 0.16$, $U_o = U_w = 2$ m/s	89

List of Figures

Figure (6.4e):	Axial velocity profiles of heavy oil-water core annular pipe flow, Engine oil ($\mu = 1060$ cP), $\alpha = 0.92$, Water loading $\psi = 0.19$, $U_o = 2$ m/s, $U_w = 2.5$ m/s	90
Figure (6.4f):	Axial velocity profiles of heavy oil-water core annular pipe flow, Engine oil ($\mu = 1060$ cP), $\alpha = 0.92$, Water loading $\psi = 0.22$, $U_o = 2$ m/s, $U_w = 3$ m/s	91
Figure (6.5a):	Turbulence Kinetic Energy k profiles of core annular pipe flow of Mineral Oil ($\mu=30$ cP) and water, $\alpha = 0.92$, $U_o = U_w = 3$ m/s	92
Figure (6.5b):	Turbulence Kinetic Energy k profiles of core annular pipe flow of Heavy Oil 5 ($\mu=256$ cP) and water, $\alpha = 0.92$, $U_o = U_w = 3$ m/s	93
Figure (6.5c):	Turbulence Kinetic Energy k profiles of core annular pipe flow of Heavy Oil 2 ($\mu=621$ cP) and water, $\alpha = 0.92$, $U_o = U_w = 3$ m/s	94
Figure (6.5d):	Turbulence Kinetic Energy k profiles of core annular pipe flow of Crude Oil 7 ($\mu=1935$ cP) and water, $\alpha = 0.92$, $U_o = U_w = 3$ m/s	94
Figure (6.5e):	Turbulence Kinetic Energy k profiles of core annular pipe flow of Heavy Oil 7 ($\mu=10230$ cP) and water, $\alpha = 0.92$, $U_o = U_w = 3$ m/s	95
Figure (6.5f):	Turbulence Kinetic Energy k profiles of core annular pipe flow of Fuel Oil ($\mu=18000$ cP) and water, $\alpha = 0.92$, $U_o = U_w = 3$ m/s	96
Figure (6.6a):	Turbulence Kinetic Energy k profiles of core annular pipe flow of Heavy Oil 5 ($\mu=256$ cP) and water, $\alpha = 0.83$, $U_o = U_w = 2$ m/s	97
Figure (6.6b):	Turbulence Kinetic Energy k profiles of core annular pipe flow of Crude Oil 7 ($\mu=1935$ cP) and water, $\alpha = 0.83$, $U_o = U_w = 2$ m/s	98
Figure (6.6c):	Turbulence Kinetic Energy k profiles of core annular pipe flow of Extra heavy oil 7 ($\mu=10230$ cP) and water, $\alpha = 0.83$, $U_o = U_w = 2$ m/s	99
Figure (6.7a):	Strain rate γ profiles development of core annular pipe flow of heavy oil 7 ($\mu=256$ cP) and water, $\alpha = 0.92$, $U_o = U_w = 3$ m/s	100
Figure (6.7b):	Strain rate γ profiles development of core annular pipe flow of heavy oil 7 ($\mu=256$ cP) and water, $\alpha = 0.92$, $U_o = U_w = 3$ m/s	100
Figure (6.7c):	Strain rate γ profiles development of core annular pipe flow of heavy oil ($\mu=1935$ cP) and water, $\alpha = 0.92$, $U_o = U_w = 3$ m/s	101
Figure (6.7d):	Strain rate γ profiles development of core annular pipe flow of extra high viscosity oil ($\mu=10230$ cP) and water, $\alpha = 0.92$, $U_o = U_w = 3$ m/s ...	102
Figure (6.8a):	Axial velocity development at oil-water interface of core annular pipe flow, Heavy oils and water, $\alpha = 0.83$, $U_o = U_w = 2$ m/s	103
Figure (6.8b):	Strain rate γ of core annular pipe flow at oil-water interface of heavy oils and water, $\alpha = 0.83$, $U_o = U_w = 2$ m/s	104
Figure (6.9a):	Turbulence kinetic energy k at oil-water interface of core annular pipe flow of heavy oils and water, $\alpha = 0.83$, $U_o = U_w = 2$ m/s.....	105

List of Figures

Figure (6.9b):	Turbulence intensity I at oil-water interface of core annular pipe flow of heavy oils and water, $\alpha = 0.83$, $U_o = U_w = 2$ m/s	105
Figure (6.9c):	Turbulence kinetic energy k at oil-water interface of core annular pipe flow of heavy oils and water, $\alpha = 0.92$, $U_o = U_w = 2$ m/s	106
Figure (6.9d):	Turbulence intensity I at oil-water interface of core annular pipe flow of heavy oils and water, $\alpha = 0.92$, $U_o = U_w = 2$ m/s	106
Figure (6.10a):	Turbulence kinetic energy k profiles development on oil-water interface of core annular pipe flow of Crude Oil1 ($\mu=530$ cP) and water, $\alpha = 0.92$, $U_o = 2$ m/s	108
Figure (6.10b):	Turbulence kinetic energy k profiles development on oil-water interface of core annular pipe flow of Engine Oil ($\mu=1060$ cP) and water, $\alpha = 0.92$, $U_o = 2$ m/s	108
Figure (6.11a):	Axial velocity at pipe centerline of core annular pipe flow of Heavy oils and water for $\alpha = 0.83$, $U_o = U_w = 2$ m/s	109
Figure (6.11b):	Axial velocity at pipe centerline of core annular pipe flow of Heavy oils and water for $\alpha = 0.92$, $U_o = U_w = 3$ m/s	110
Figure (6.12a):	Development of wall shear stress τ of core annular pipe flow of Heavy oils and water, $\alpha = 0.92$, $U_o = U_w = 3$ m/s	111
Figure (6.12b):	Friction coefficient C_f of core annular pipe flow of heavy oils and water, $\alpha = 0.92$, $U_o = U_w = 3$ m/s	112
Figure (6.13a):	Plot of static pressure p along the pipe length for core annular pipe flow of Heavy oil ($\mu=1935$ cP) and water, $\alpha = 0.92$, $U_o = U_w = 3$ m/s..	113
Figure (6.13b):	Plot of static pressure p along the pipe length for core annular pipe flow of Heavy oils and water, $\alpha = 0.92$, $U_o = U_w = 2$ m/s	114
Figure (6.13c):	Plot of static pressure p along pipeline length for core annular pipe flow of Heavy oils and water, $\alpha = 0.92$, $U_o = U_w = 2$ m/s	114
Figure (6.14a):	Pressure gradient (dP/dx) as function of water loading ψ , Core annular pipe flow Heavy oils and water, $\alpha=0.96$	117
Figure (6.14b):	Pressure gradient ratio ϕ as function of water loading ψ , Core annular pipe flow Heavy oils and water, $\alpha=0.96$	117
Figure (6.15a):	Pressure gradient (dp/dx) as function of water loading ψ , Core annular pipe flow of Heavy oil ($\mu=530$) and water, Different α	119
Figure (6.15b):	Pressure gradient (dp/dx) as function of water loading ψ , Core annular pipe flow of Heavy oils ($\mu=530$ and 1060 cP) and water, Different α	119
Figure (6.16a):	Friction coefficient C_f as function of water loading ψ , Core annular pipe flow of Heavy oils ($\mu=530$ and 1060 cP) and water, $\alpha=0.92$	121

List of Figures

Figure (6.16b):	Friction coefficient ratio β as function of water loading ψ , Core annular pipe flow of Heavy oils ($\mu=530$ and 1060 cP) and water, $\alpha=0.92$	121
Figure (6.17a):	Friction coefficient C_f as function of water loading ψ , Core annular pipe flow of Crude Oil 1 ($\mu=530$ cP) and water, $\alpha = 0.96, 0.92$ and 0.83	122
Figure (6.17b):	Friction coefficient ratio β as function of water loading ψ , Core annular pipe flow of Heavy oils ($\mu=530$ and 1060 cP) and water, $\alpha=0.96, 0.92$, and 0.83	123
Figure (6.18a):	Pressure gradient (dp/dx) as function of oil superficial velocity, Core annular pipe flow of Engine Oil ($\mu=1060$ cP) and water, $\alpha = 0.96, 0.92$ and 0.83	125
Figure (6.18b):	Pressure gradient (dp/dx) as function of oil Reynolds number (Re_o), Core annular pipe flow of Engine Oil ($\mu=1060$ cP) and water, $\alpha = 0.96, 0.92$ and 0.83	125
Figure (6.18c):	Pressure gradient (dp/dx) as function of oil Reynolds number (Re_o), Core annular pipe flow of Engine Oil ($\mu=1060$ cP) and water, $\alpha = 0.96, 0.92$ and 0.83	126
Figure (6.19a):	Friction coefficient C_f as function of oil superficial velocity (U_{so}), Core annular pipe flow of Engine Oil ($\mu=1060$ cP) and water, $\alpha = 0.96, 0.92$ and 0.83	127
Figure (6.19b):	Friction coefficient C_f as function of oil Reynolds number (Re_o), Core annular pipe flow of Engine Oil ($\mu=1060$ cP) and water, $\alpha = 0.96, 0.92$ and 0.83	128
Figure (6.19c):	Friction coefficient ratio β as function of oil Reynolds number (Re_o), Core annular pipe flow of Engine Oil ($\mu=1060$ cP) and water, $\alpha = 0.96, 0.92$ and 0.83	128
Figure (6.20a):	Pressure gradient as function of oil/water viscosity ratio μ_r for the core annular pipe flow of different oils and water, $\alpha = 0.96$	130
Figure (6.20b):	Pressure gradient ratio ϕ as function of oil/water viscosity ratio μ_r for the core annular pipe flow of different oils and water, $\alpha = 0.96$	130
Figure (6.20c):	Pressure gradient ratio ϕ as function of oil/water viscosity ratio μ_r for the core annular pipe flow of different oils and water, $\alpha = 0.96, 0.92$, and 0.83	131
Figure (6.21a):	Pressure gradient dp/dx as function of oil Reynolds number (Re_o) for the core annular pipe flow of different oils and water, $\alpha = 0.96$	132
Figure (6.21b):	Pressure gradient ratio ϕ as function of oil Reynolds number (Re_o) for the core annular pipe flow of different oils and water, $\alpha = 0.96$	132

List of Figures

Figure (6.21c):	Pressure gradient ratio ϕ as function of oil Reynolds number $(Re)_o$ for the core annular pipe flow of different oils and water, $\alpha = 0.96, 0.92,$ and 0.83	133
Figure (6.22a):	Friction coefficient C_f as function of oil/water viscosity ratio μ_r for the core annular pipe flow of different oils and water, $\alpha = 0.96$	134
Figure (6.22b):	Friction coefficient ratio β as function of oil/water viscosity ratio μ_r for the core annular pipe flow of different oils and water, $\alpha = 0.96$	135
Figure (6.22c):	Friction coefficient C_f as function of oil/water viscosity ratio μ_r for the core annular pipe flow of different oils and water, $\alpha = 0.96, 0.92,$ and 0.83	135
Figure (6.22d):	Friction coefficient ratio β as function of oil/water viscosity ratio μ_r for the core annular pipe flow of different oils and water, $\alpha = 0.96, 0.92,$ and 0.83	136
Figure (6.23a):	Friction coefficient C_f as function of oil's Reynolds number $(Re)_o$ for the core annular pipe flow of different oils and water, $\alpha = 0.96$	137
Figure (6.23b):	Friction coefficient ratio β as function of oil's Reynolds number $(Re)_o$ for the core annular pipe flow of different oils and water, $\alpha = 0.96$	138
Figure (6.23c):	Friction coefficient C_f as function of oil's Reynolds number $(Re)_o$ for the core annular pipe flow of different oils and water, $\alpha = 0.96, 0.92,$ and 0.83	138
Figure (6.23d):	Friction coefficient ratio β as function of oil's Reynolds number $(Re)_o$ for the core annular pipe flow of different oils and water, $\alpha = 0.96, 0.92,$ and 0.83	139
Figure (6.24a):	Pumping power P as function of water loading ψ for core annular pipe flow of Engine Oil ($\mu=1060$ cP) and water, $\alpha=0.96, 0.92,$ and 0.83	141
Figure (6.24b):	Pumping power reduction $\%PR$ as function of water loading ψ for core annular pipe flow of Engine Oil ($\mu=1060$ cP) and water, $\alpha = 0.96, 0.92,$ and 0.83	142
Figure (6.25a):	Pumping power P as function of oil Reynolds number $(Re)_o$ for core annular pipe flow of Engine Oil ($\mu=1060$ cP) and water, $\alpha = 0.96, 0.92,$ and 0.83	143
Figure (6.25b):	Pumping power reduction $\% PR$ as function of oil Reynolds number $(Re)_o$ for core annular pipe flow of Engine Oil ($\mu=1060$ cP) and water, $\alpha = 0.96, 0.92,$ and 0.83	144
Figure (6.26a):	Pumping power P as function of oil/water viscosity ratio μ_r for the core annular pipe flow of different oils and water, $\alpha = 0.96, 0.92,$ and 0.83	145

List of Figures

Figure (6.26b):	Pumping power reduction $PR\%$ as function of oil/water viscosity ratio μ_r for the core annular pipe flow of different oils and water, $\alpha = 0.96, 0.92, \text{ and } 0.83$	146
Figure (6.27a):	Pumping power as function of oil Reynolds number $(Re)_o$ for the core annular pipe flow of different oils and water, $\alpha = 0.96, 0.92, \text{ and } 0.83$	147
Figure (6.27b):	Pumping power reduction $PR\%$ as function of oil Reynolds number $(Re)_o$ for the core annular pipe flow of different oils and water, $\alpha = 0.96, 0.92, \text{ and } 0.83, U_o=U_w=2 \text{ and } 3 \text{ m/s}$	148
Figure (6.27c):	Pumping power reduction $PR\%$ as function of oil Reynolds number $(Re)_o$ for the core annular pipe flow of different oils and water, $\alpha = 0.96, 0.92, \text{ and } 0.83, U_o=U_w=2 \text{ and } 3 \text{ m/s}$	149

List of Tables

Table (3.1):	Standard k - ω constants [Wilcox (1998)]	41
Table (4.1):	Summary of meshing data for the three flow configurations	53
Table (6.1):	Heavy oils viscosity and density.....	66
Table (6.2):	Reynolds numbers of core annular pipe flow of oil-water system for Figures (6.1)	67
Table (6.3):	Reynolds numbers of core annular pipe flow of oil-water system for Figures (6.2)	74
Table (6.4):	Reynolds numbers of core annular pipe flow of oil-water system for Figures (6.3)	80
Table (6.5):	Reynolds numbers of core annular pipe flow of oil-water system for Figures (6.4)	85
Table (6.6):	Reynolds numbers of core annular pipe flow of oil-water system for Figures (6.5)	92
Table (6.7):	Reynolds numbers of core annular pipe flow of oil-water system for Figures (6.6)	97
Table (6.8):	Reynolds numbers of core annular pipe flow of oil-water system for Figures (6.7)	99

العنوان:	Heavy Oils Flow in Pipes
المؤلف الرئيسي:	Sakr, Ahmed Lotfy Hassan Rabie
مؤلفين آخرين:	Mousa, Mohamed Ghassoub Saafan, Sultan, Gamal Ibrahim, Talba, Mohamed Abd Almotelb(Super.)
التاريخ الميلادي:	2013
موقع:	المنصورة
الصفحات:	1 - 160
رقم MD:	537574
نوع المحتوى:	رسائل جامعية
اللغة:	Arabic
الدرجة العلمية:	رسالة ماجستير
الجامعة:	جامعة المنصورة
الكلية:	كلية الهندسة
الدولة:	مصر
قواعد المعلومات:	Dissertations
مواضيع:	هندسة القوى الميكانيكية، الزيوت الثقيلة، الأنابيب الموصلة، القوى الميكانيكية
رابط:	https://search.mandumah.com/Record/537574



جامعة المنصورة
كلية الهندسة
هندسة القوى الميكانيكية

سريان الزيوت الثقيلة في الأنابيب

رسالة مقدمة من

مهندس / أحمد لطفي حسن ربيع صقر

بكالوريوس في هندسة القوى الميكانيكية ٢٠٠٥م

إلى كلية الهندسة جامعة المنصورة
لاستكمال متطلبات الحصول على درجة الماجستير
في هندسة القوى الميكانيكية

تحت إشراف

أ. د. محمد غصوب سعفان موسى
أستاذ - هندسة القوى الميكانيكية
كلية الهندسة - جامعة المنصورة

أ. د. جمال إبراهيم أحمد سلطان
أستاذ - هندسة القوى الميكانيكية
كلية الهندسة - جامعة المنصورة

د. محمد عبد المطلب طلبت
مدرس منفرد - هندسة القوى الميكانيكية
كلية الهندسة - جامعة المنصورة

٢٠١٣م

*Mansoura University
Faculty of Engineering
Mechanical Power Engineering Dept.*



Heavy Oils Flow in Pipes

by

Eng. Ahmed Lotfy Hassan Rabie Sakr

B.Sc. Mechanical Power Engineering 2005

A Thesis

Submitted to the Faculty of Engineering, Mansoura University
in Partial Fulfillment of the Requirements for the
Degree of Master of Science (M.Sc.)

in

Mechanical Power Engineering

Supervised by

Prof. Dr. Gamal Ibrahim Sultan
Professor
Mechanical Engineering Dept.
Mansoura University

Prof. Dr. Mohamed Ghassob Mousa
Professor
Mechanical Engineering Dept.
Mansoura University

Dr. Mohamed Abdel Motelb Tolba
Assistant Professor, Mechanical Engineering Dept.
Mansoura University

2013